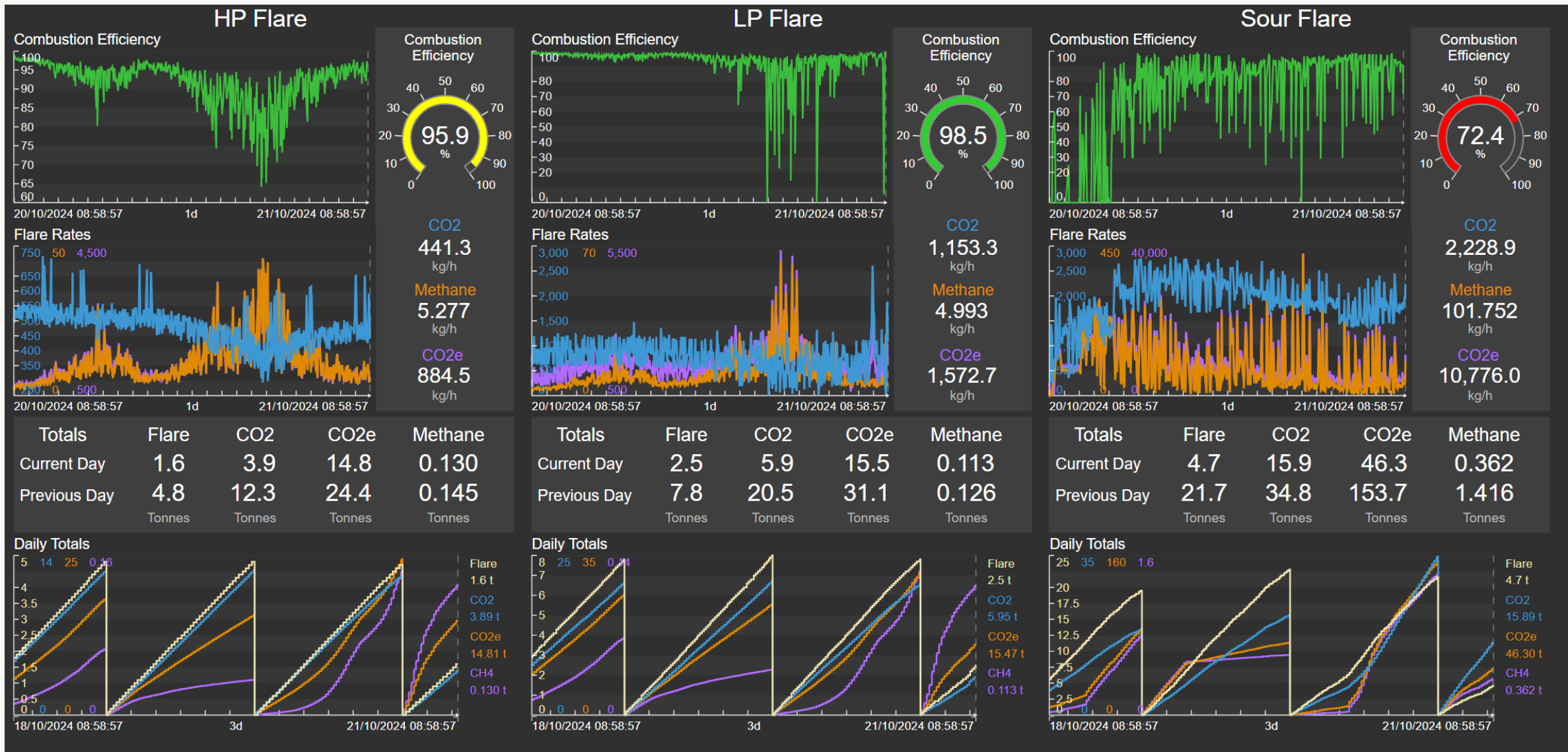




Juan Martin Rodriguez, Bob Peebles

Flare Gas Composition and Destruction Efficiency using Accord's CHARM and Combustor

Combustor Baseline Functionality



Combustor Baseline Functionality

- Minute by minute calculation of CO₂, CH₄, CO₂e flow rates and cumulative totals
- Live uncertainty reporting for Combustion Efficiency
- Identify and optimise CO₂e performance (where plant configuration allows)
- Ability to post process data for mismeasurement events and for verification checks (e.g., fuel gas composition)
- Can be updated to study, inform and incorporate future plant changes
- Pre and post combustion compositional information such as ISO6976 CVs, AGA8 Densities, etc.



Combustor Updates

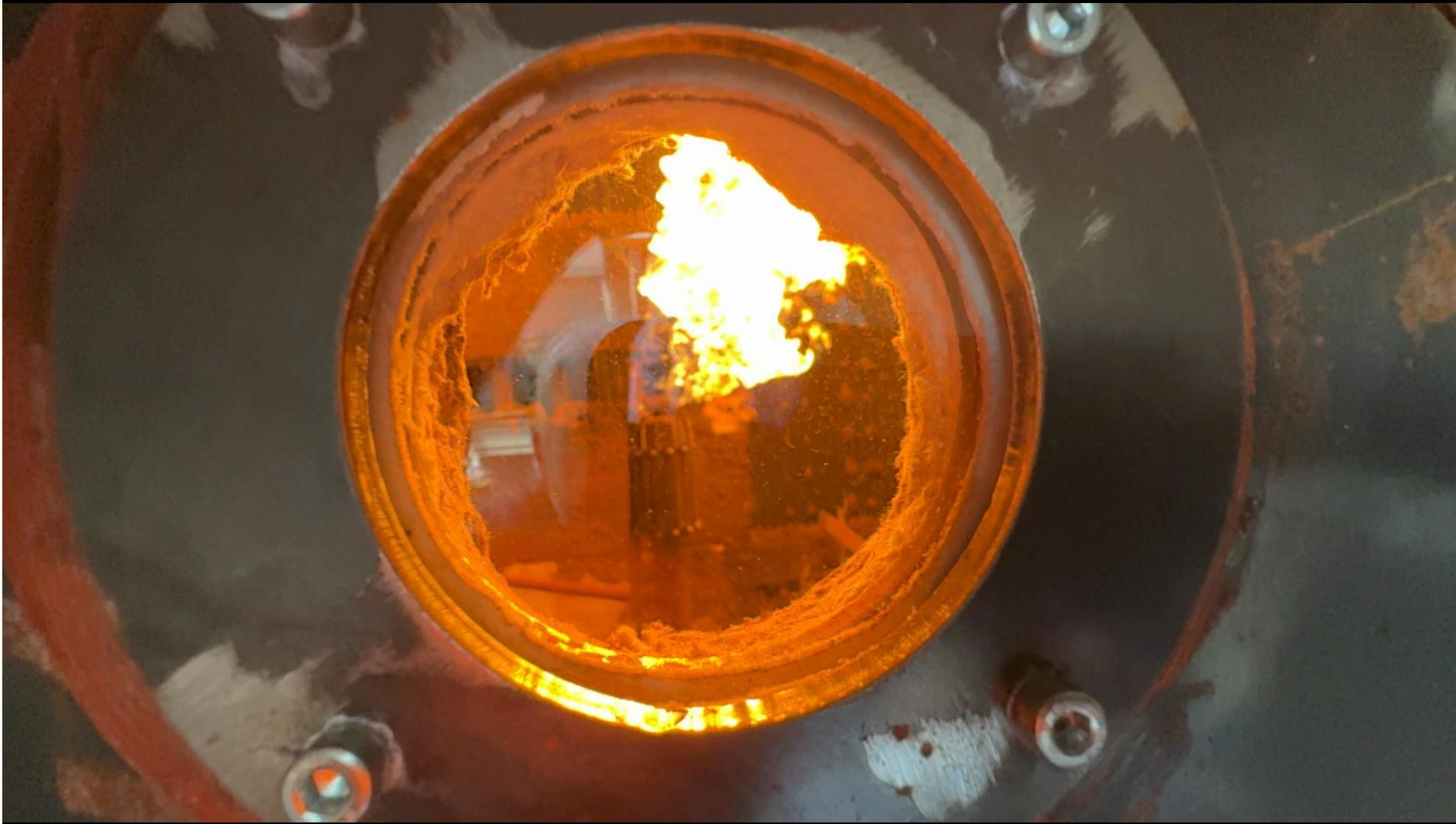
- Flare Testing with Greens Combustion and TotalEnergies
- Flare test facility uncertainty calculations have been developed
- Destruction Efficiency (DE) calculation developed from results of flare testing
- DE calculation and reporting in CO2e terms has been implemented in Combustor
- DE uncertainty calculations have been implemented in Combustor
- CO2e uncertainty calculations for CE have been developed and will be modified to use DE as the baseline
- Speed of Sound Verification Check and Reconciliation (SOS VCR) functionality is being developed



Bari Flare Testing



Bari Flare Testing

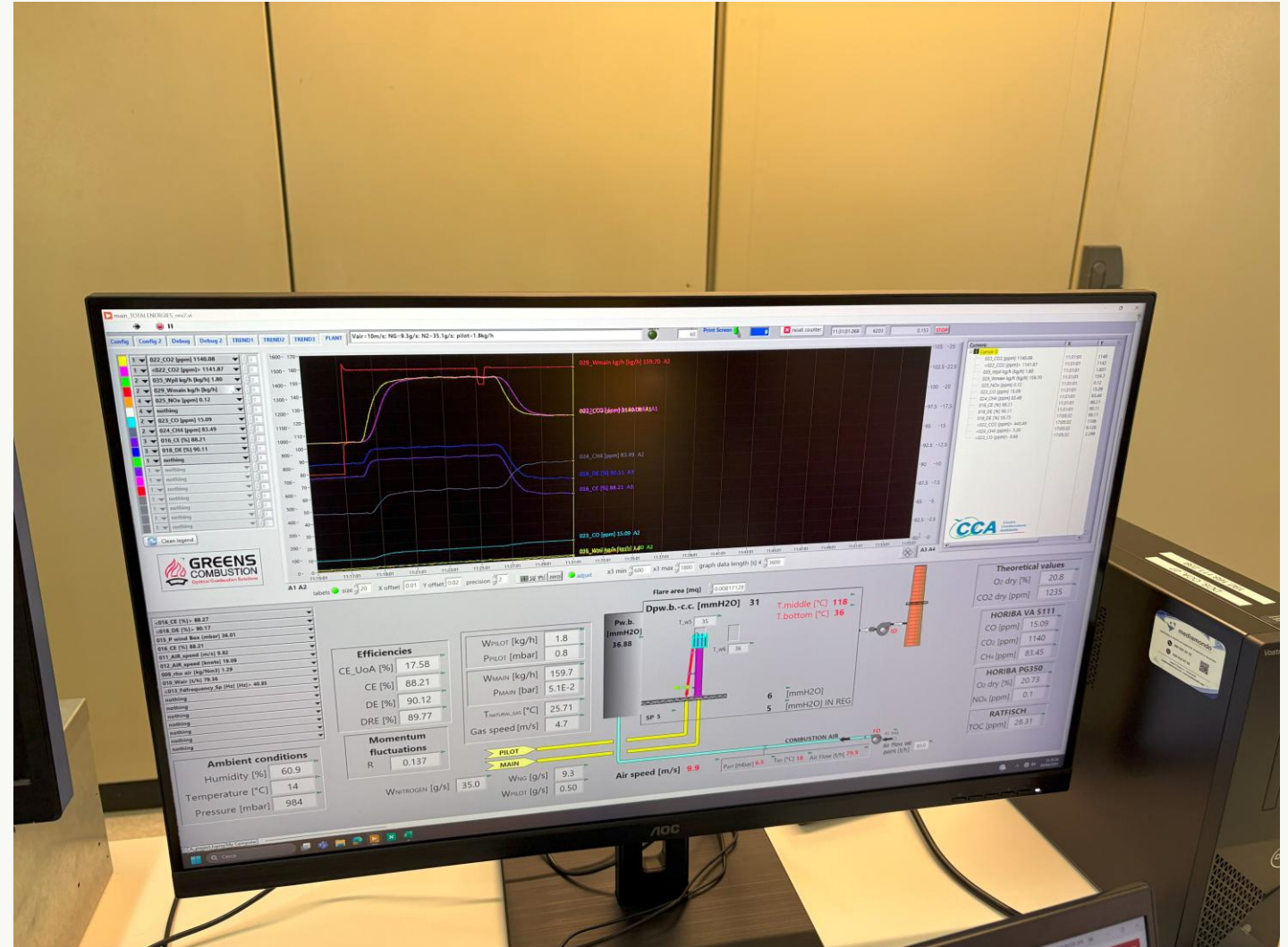


Bari Flare Testing

The Greens Combustion test facility located in Bari, Italy utilises an operator configurable data acquisition and control system which is connected to an array of measurement and analytical instruments.

Pre-designed test matrices are managed by a dedicated control room team, and each test is given a unique identifier and data is date and time stamped.

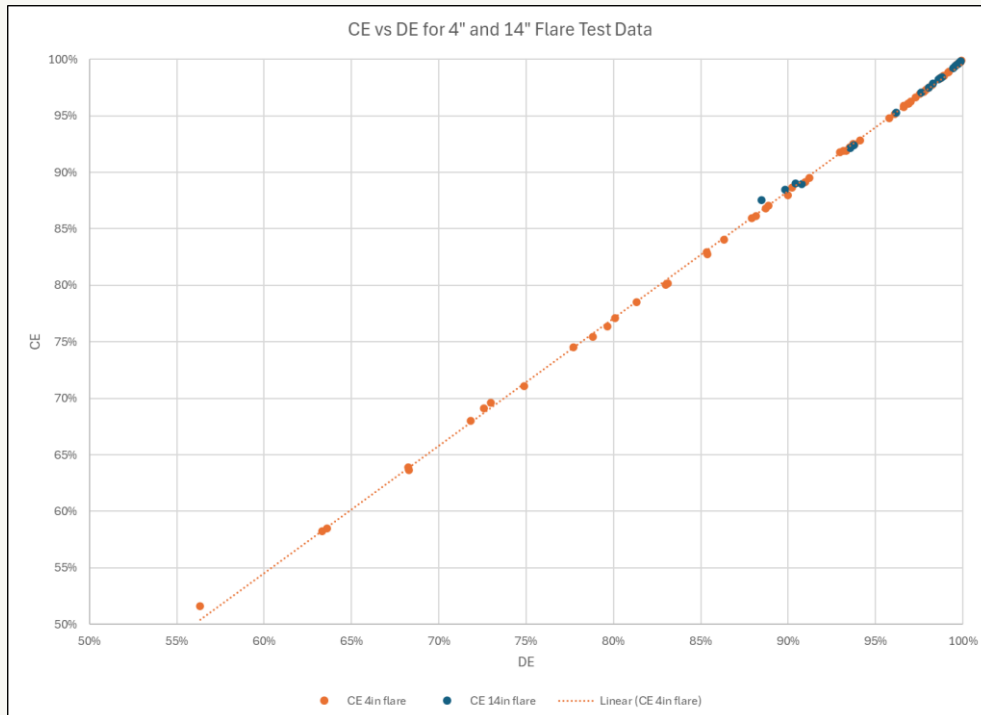
Measurement and analytical equipment is regularly calibrated. Natural gas used for testing is obtained from the local supply grid and regularly analysed.



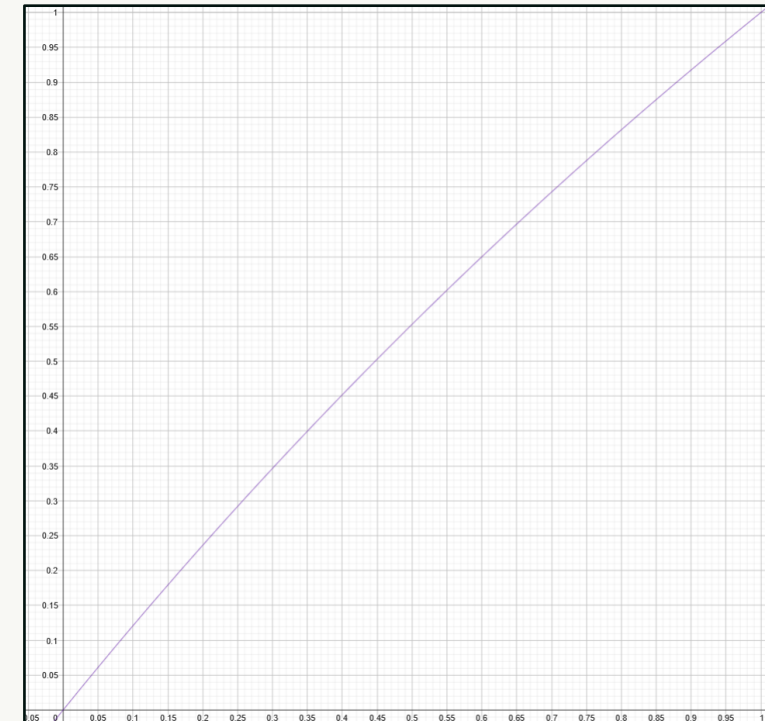
Destruction Efficiency

Based on test results from the Greens Combustion facility we have been able to develop a relationship between Destruction Efficiency (DE) and Combustion Efficiency (CE) – which, in simple terms, means that we can now calculate DE, and the associated uncertainty of DE, within Combustor.

CE versus DE from 4-inch and 14-inch Flare Test Data

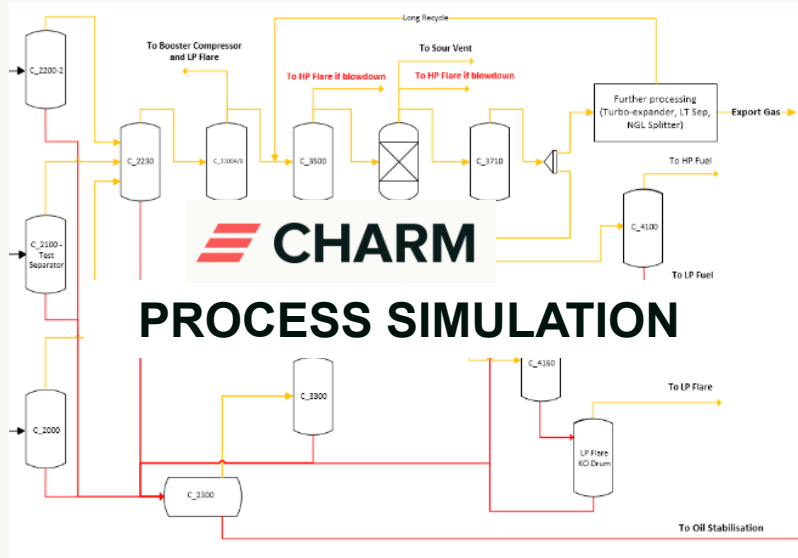


Full Fit of CE and DE data



CHARM VoS VCR

Reconcile the flare gas composition when a significant difference in VoS is observed between the USM, samples and Combustor. CHARM VoS VCR incorporates all relevant information available.

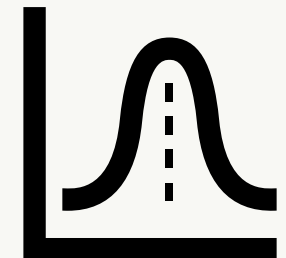


Component	Mole %	Normalised Mole %
Oxyg.	0.0025	0.0025
Nitrogen	0.2828	0.2804
Carbon Dioxi	3.8133	3.7816
Methane	84.280	84.4202
Ethane	7.6905	7.6905
Propane	2.2557	2.2557
I-Butane	1.2618	1.2618
N-Butane	0.5152	0.5152
Neo-Pentane	0.0010	0.0010
I-Pentane	0.1175	0.1165

LATEST SAMPLES

Heptanes	0.1679	0.1665
Octanes	0.0134	0.0133
Nonanes	0.0426	0.0422
Decanes	0.1245	0.1235
Total	100.8385	100.0000

- **Reconciled Flare Gas composition**
- **Reconciled SOS**

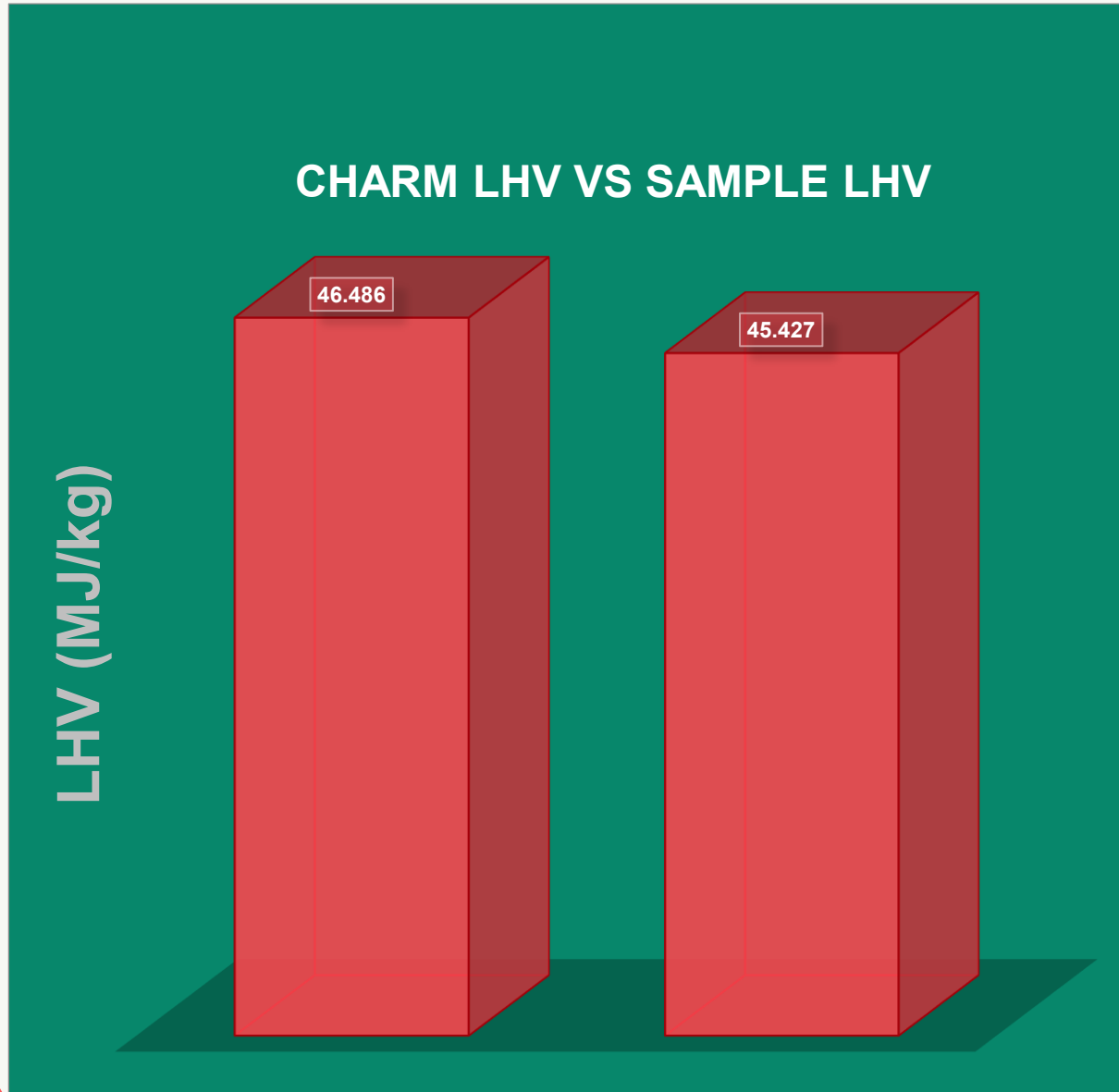


Accord and Data Reconciliation

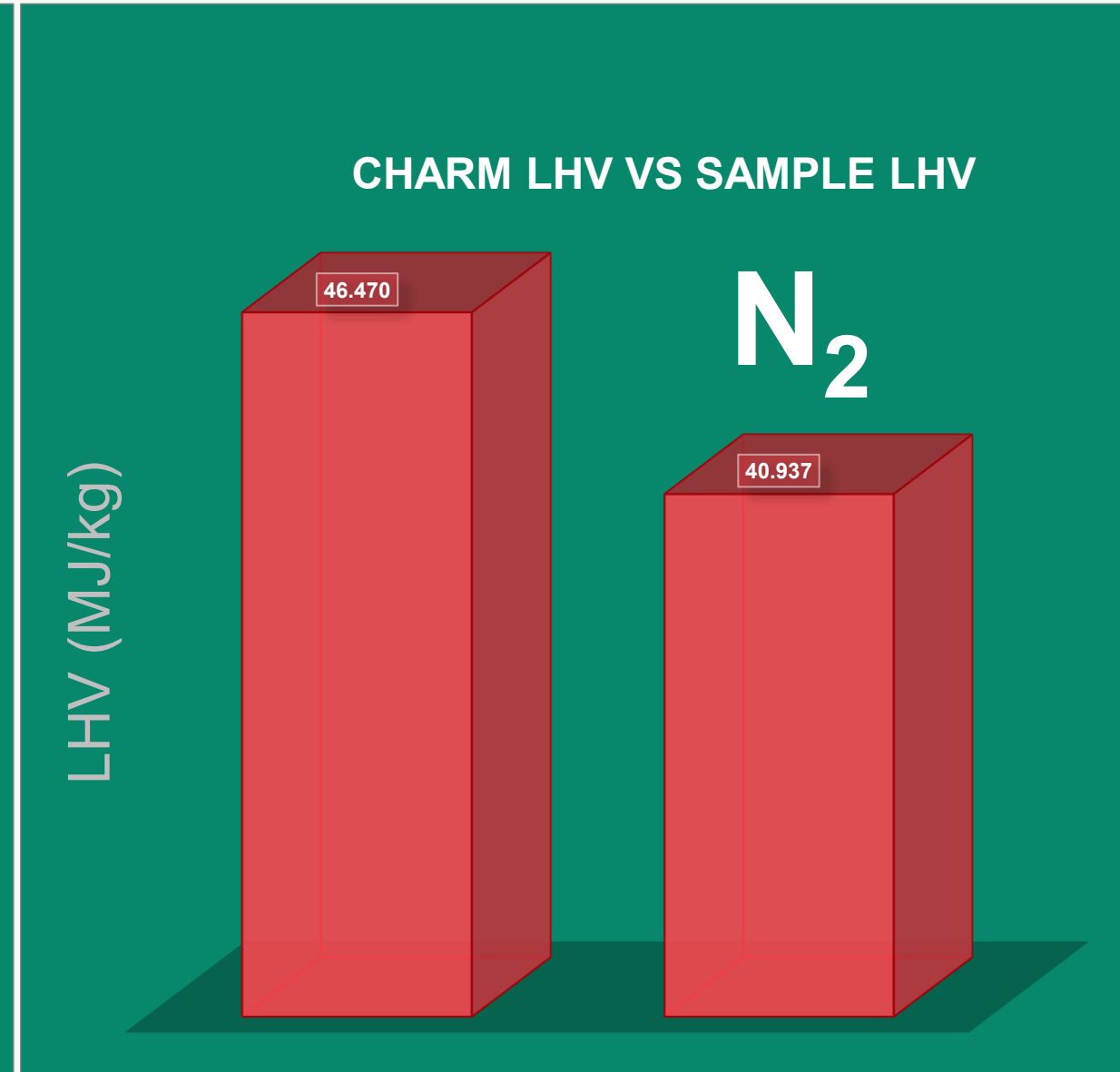
- Papers
 - PUFMW 2008: Experiences in the Use of Uncertainty Based Allocation in a North Sea Offshore Oil Allocation System
 - NSFMW 2011: Gross Meter Error Detection and Elimination by Data Reconciliation
 - NSFMW 2013: Allocation in an Uncertain World: Maximising the Use of Data with UBA on Global Producer III
 - NSFMW 2019: Data Reconciliation in Microcosm – Reducing DP Meter Uncertainty. Oculus European Patent Awarded 2024
- Projects with successful application
 - UBA in ExxonMobil's Beryl Area offshore oil allocation system
 - MAERSK: Allocation of oil and gas between the Dumbarton and Lochranza fields produced across Maersk's Global Producer III (GP III) FPSO (Floating Production Storage and Offloading)
 - REPSOL: Introduced UBA to the Flotta pipeline system 2024



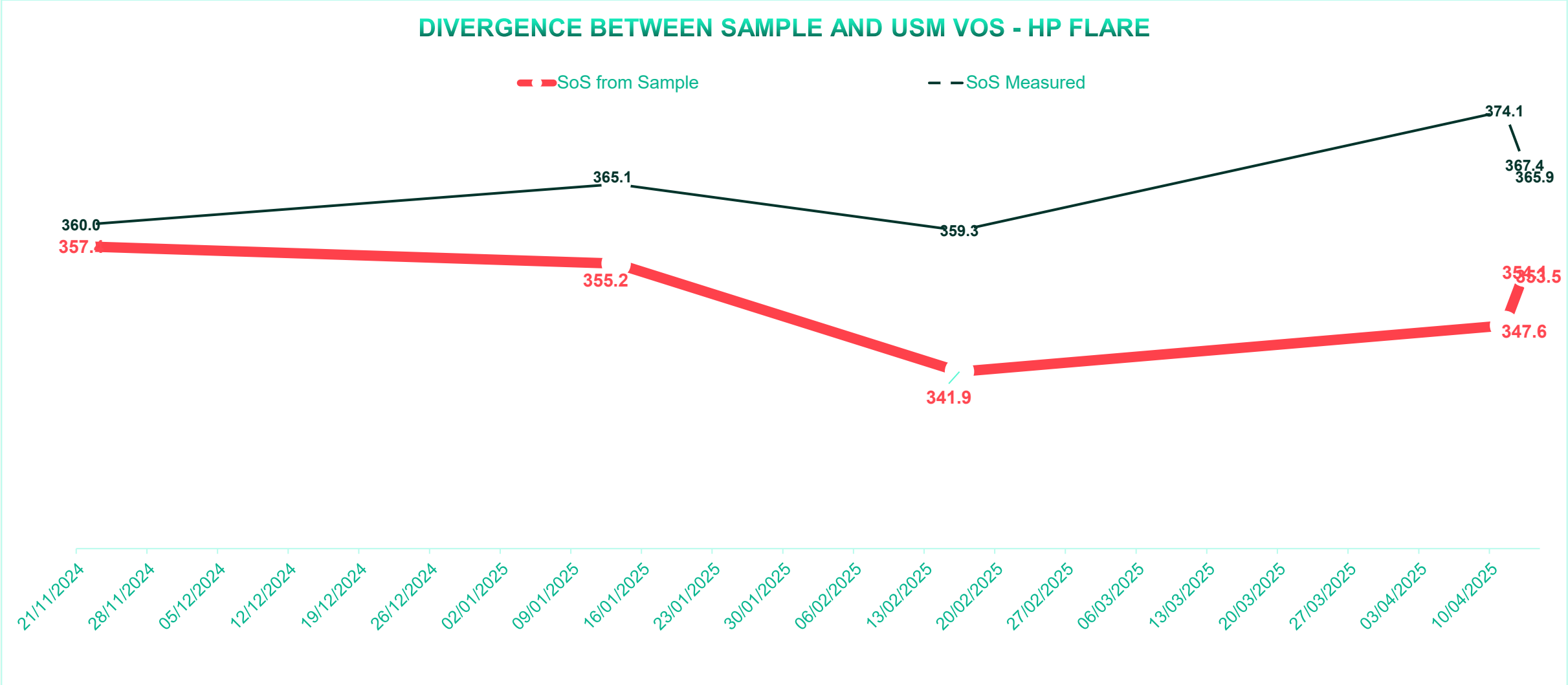
HP Flare - LHV



LP Flare - LHV



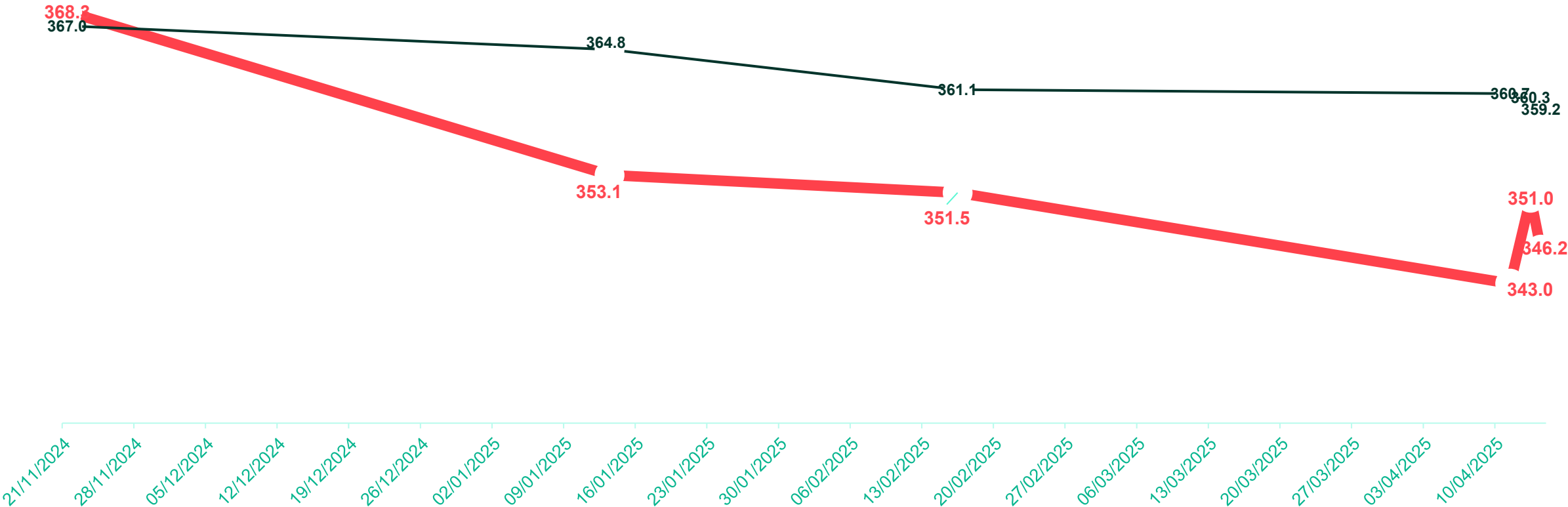
HP Flare – Measured VoS vs Sample VoS



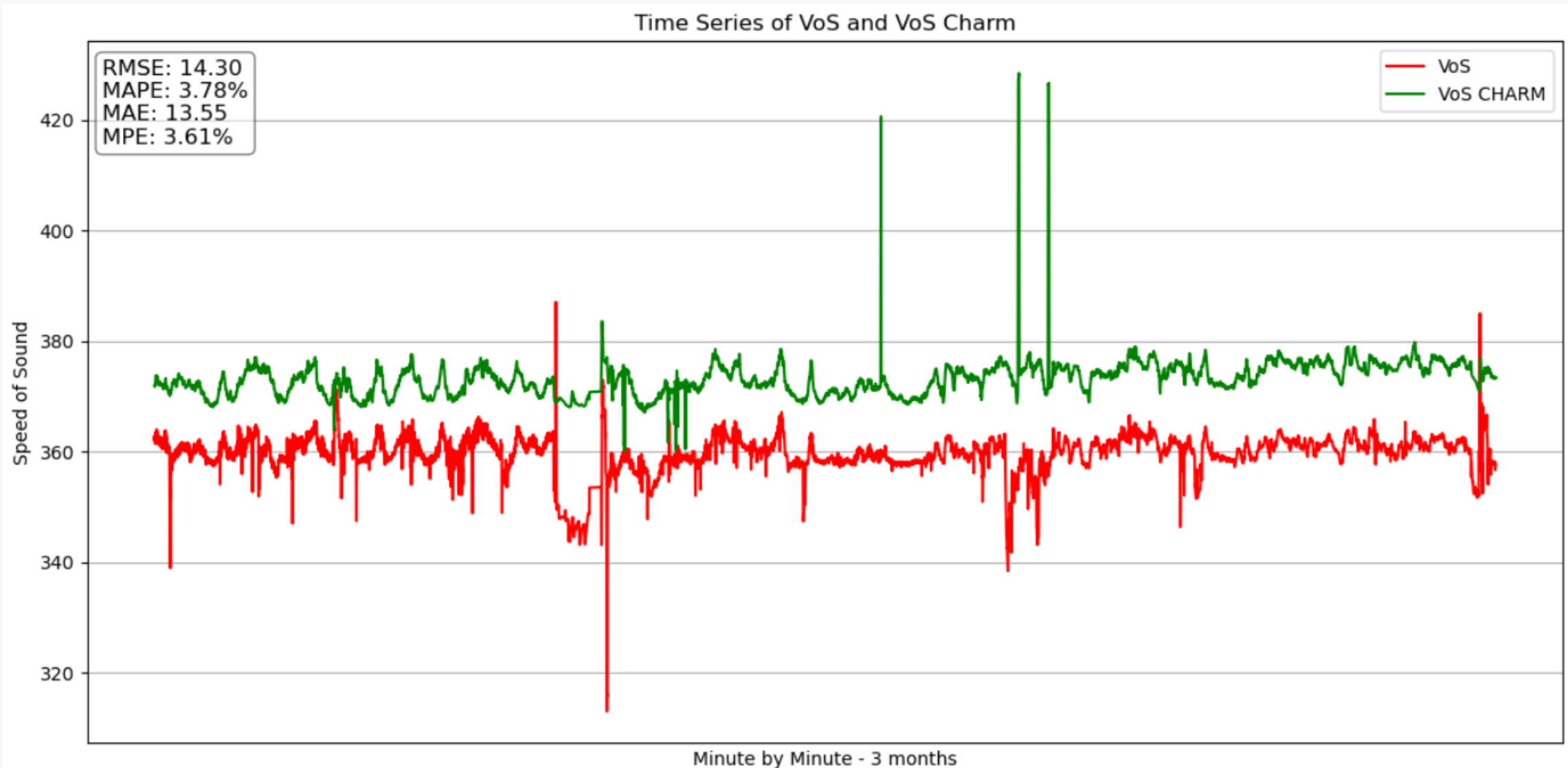
LP Flare – Measured VoS vs Sample VoS

DIVERGENCE BETWEEN SAMPLE AND USM SOS - LP FLARE

SoS from Sample m/s SoS Measured m/s



LP Flare - Measured VoS vs CHARM VoS



VoS VCR Example Case

Other unknown sources

N2	-
CO2	-
CH4	-
C2+	-

 **CHARM**

Unknown Seal Gas Flowrate & Comp

N2	52.4%
CO2	14.7%
CH4	0.0%
C2+	32.8%

 **CHARM**

CHARM HC Stream Flowrate & Comp

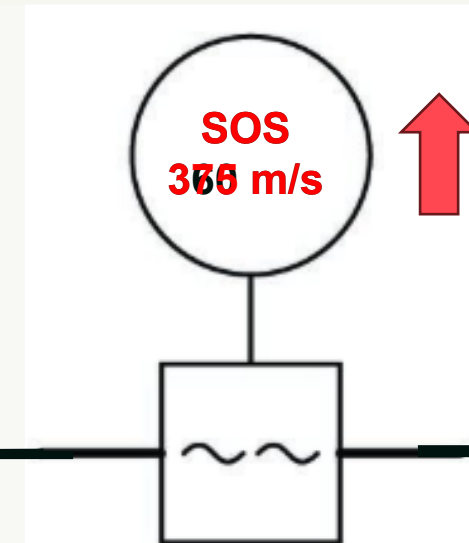
N2	0.4%
CO2	3.0%
CH4	80.5%
C2+	16.1%

N2	4.8%
CO2	3.4%
CH4	75.7%
C2+	16.0%

VoS 

Constrained nonlinear optimization used for data reconciliation

Levenberg–Marquardt algorithm



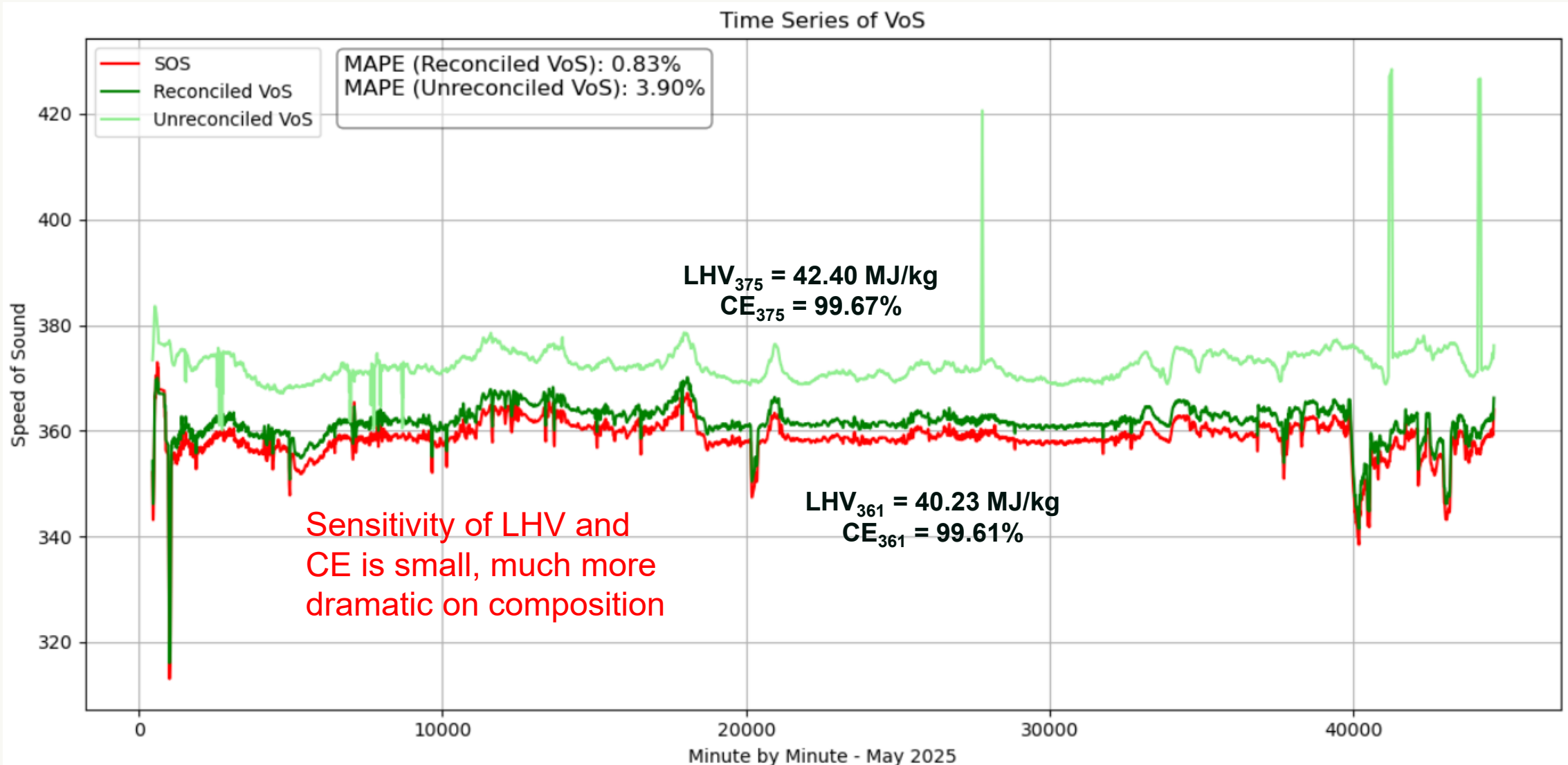
 **COMBUSTOR**

Sensitivity of LHV and CE is small, much more dramatic on composition

$LHV_{361} = 40.23 \text{ MJ/kg}$
 $CE_{361} = 99.61\%$

$LHV_{375} = 42.40 \text{ MJ/kg}$
 $CE_{375} = 99.67\%$

VoS VCR – LP Flare





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